

**Amendments to the Claims:**

Claim 1 (Original) A process for producing stable lubricant bright stock comprising the steps of:

- a) providing a petroleum residuum-derived stream having a sulfur content of less than 1% and a nitrogen content of less than 0.5%;
- b) separating the residuum-derived stream at a distillation cut point in the range of 1150°F to 1300°F, into a heavy fraction and at least one light fraction;
- c) hydrocracking the at least one light fraction under lube hydrocracking in a lube hydrocracking zone in the presence of a hydrocracking catalyst and hydrogen under conditions to reduce the concentration of sulfur and nitrogen to suitable levels for hydroisomerization dewaxing; and
- d) dewaxing at least a portion of the hydrocracked stream in an hydroisomerization zone in the presence of a hydroisomerization catalyst and hydrogen under hydroisomerization conditions to produce a lubricant bright stock.

Claim 2 (Original) The process of Claim 1, wherein the petroleum residuum-derived stream is a hydrocracked deasphalted oil.

Claim 3 (Original) The process of Claim 1, wherein the petroleum residuum-derived stream is a hydrocracked residuum.

Claim 4 (Original) The process of Claim 1, wherein the petroleum residuum-derived stream has a concentration of sulfur of less than 0.5% and a concentration of nitrogen of less than 0.2%.

- Claim 5 (Original) The process of Claim 1, further comprising stabilizing the lubricant bright stock in a hydrofinishing zone in the presence of a hydrofinishing catalyst and hydrogen under hydrofinishing conditions.
- Claim 6 (Original) The process of Claim 5, further comprising contacting the stabilized lubricant bright stock with clay in a clay treatment zone.
- Claim 7 (Original) The process of Claim 1, wherein the bright stock has a viscosity, measured at 100°C, of greater than 15 cSt and viscosity index of greater than 80.
- Claim 8 (Original) The process of Claim 7, wherein the bright stock has a viscosity index of greater than 90.
- Claim 9 (Original) The process of Claim 1, wherein the bright stock has a viscosity in the range of 20 and 60 cSt, measured at 100°C.
- Claim 10 (Original) The process according to Claim 1, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SAPO-31, SAPO-41, SM-3, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57, SSZ-32, offretite, ferrierite and combinations thereof.
- Claim 11 (Original) The process according to Claim 10, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SAPO-31, SM-3, SSZ-32, and ZSM-23.
- Claim 12 (Original) The process according to Claim 11, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SM-3, SSZ-32, and ZSM-23.
- Claim 13 (Original) The process according to Claim 1, wherein the hydroisomerization catalyst has a metal hydrogenation component.

- Claim 14 (Original) The process according to Claim 13, wherein the metal hydrogenation component is platinum, palladium, or a mixture thereof.
- Claim 15 (Currently Amended) The process according to Claim ~~40~~ 14 wherein the metal hydrogenation component is platinum.
- Claim 16 (Original) The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 50 ppm and a concentration of sulfur of less than 100 ppm.
- Claim 17 (Original) The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 30 ppm and a concentration of sulfur of less than 50 ppm.
- Claim 18 (Original) The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 10 ppm and a concentration of sulfur of less than 20 ppm.